

# Structured packings for the internal Heat Integration in Distillation Columns (HIDiC)

R. Sumbharaju  
E.R van Selow  
A. de Groot  
D.F. Meyer  
O.S.L. Bruinsma

August 2015  
ECN-L--15-070





# Structured packings for the internal Heat Integration in Distillation Columns (HIDiC)

## Author

R. Sumbharaju, E.R van Selow\*, A.de Groot,  
D. F. Meyer, O.S.L. Bruinsma

\*Corresponding author: vanselow@ecn.nl

## Background & Concept

### Why?

- Energy use of distillation is 40 % of the total in the chemical and refinery industries (=180 PJ/y in the Netherlands)
- Separation of close boiling liquid mixtures are highly energy intensive (such typical column uses 90 MW of energy)
- The HIDiC concept was introduced to radically improve the energy efficiency
- Determine mass and heat transfer coefficients
- Determine the optimum operating conditions
- Assess the economic viability

### How?

- Concept of Vapor recompression (VRC) are already known [1] see Figure 1
- In HIDiC [2]
  - Vapor leaving the stripping is compressed before entering rectifier
  - Rectifier operates at higher temperature/Pressure to allow heat integration between rectifying and stripping
  - Reversibility of the column can be increased by upgrading the heat rejected in rectification section and transferring it to stripping section

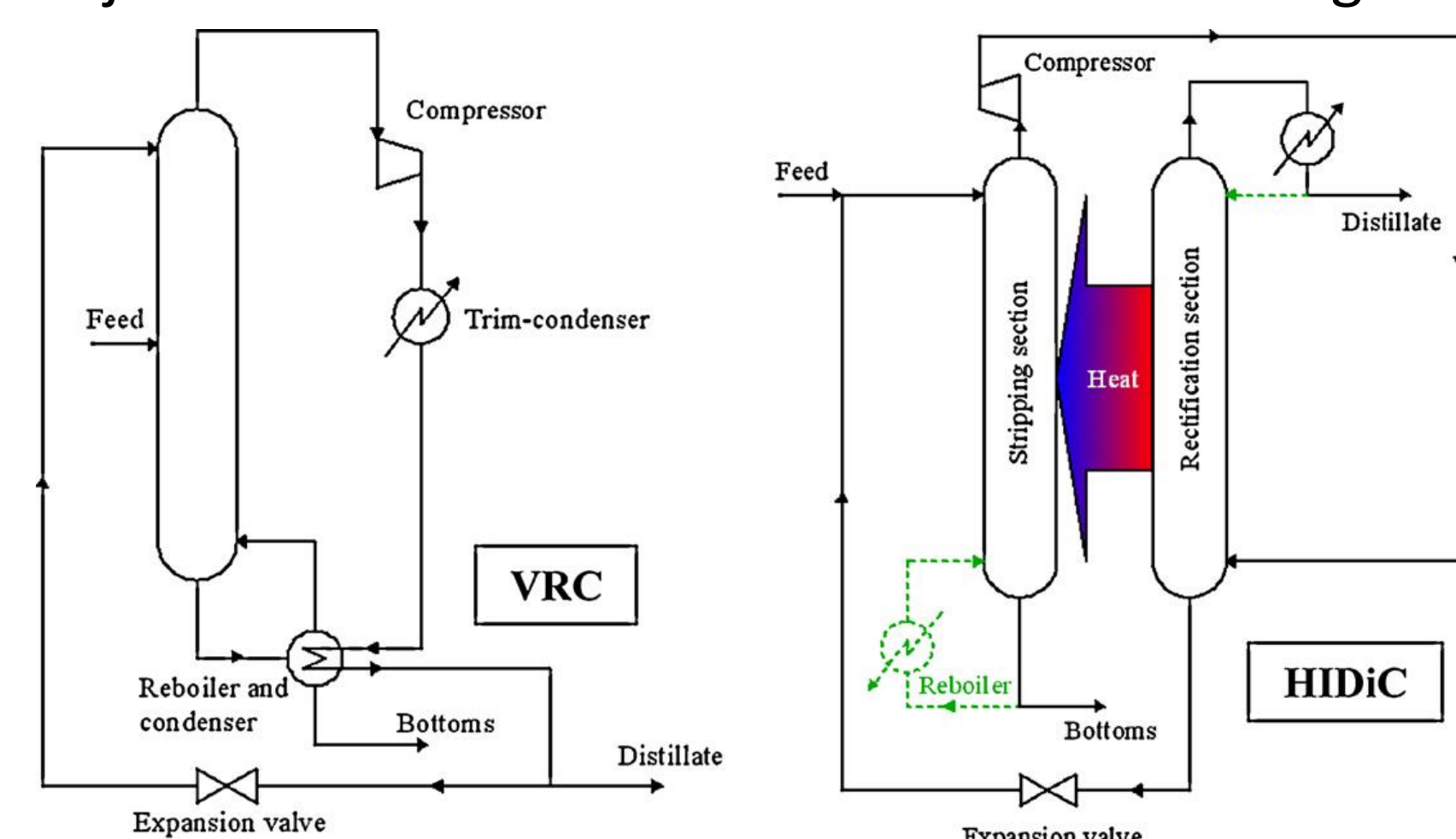


Figure 1: The VRC and HIDiC column

## Experimental set-up

- This structured HIDiC contains 3 sections (Figure 2)
- Basic unit of plate packing HIDiC consists of two layers of 5 stacked corrugated sheets (0.2m X 0.2m) of Mellapak 350.Y (Sulzer) (Figure 3)

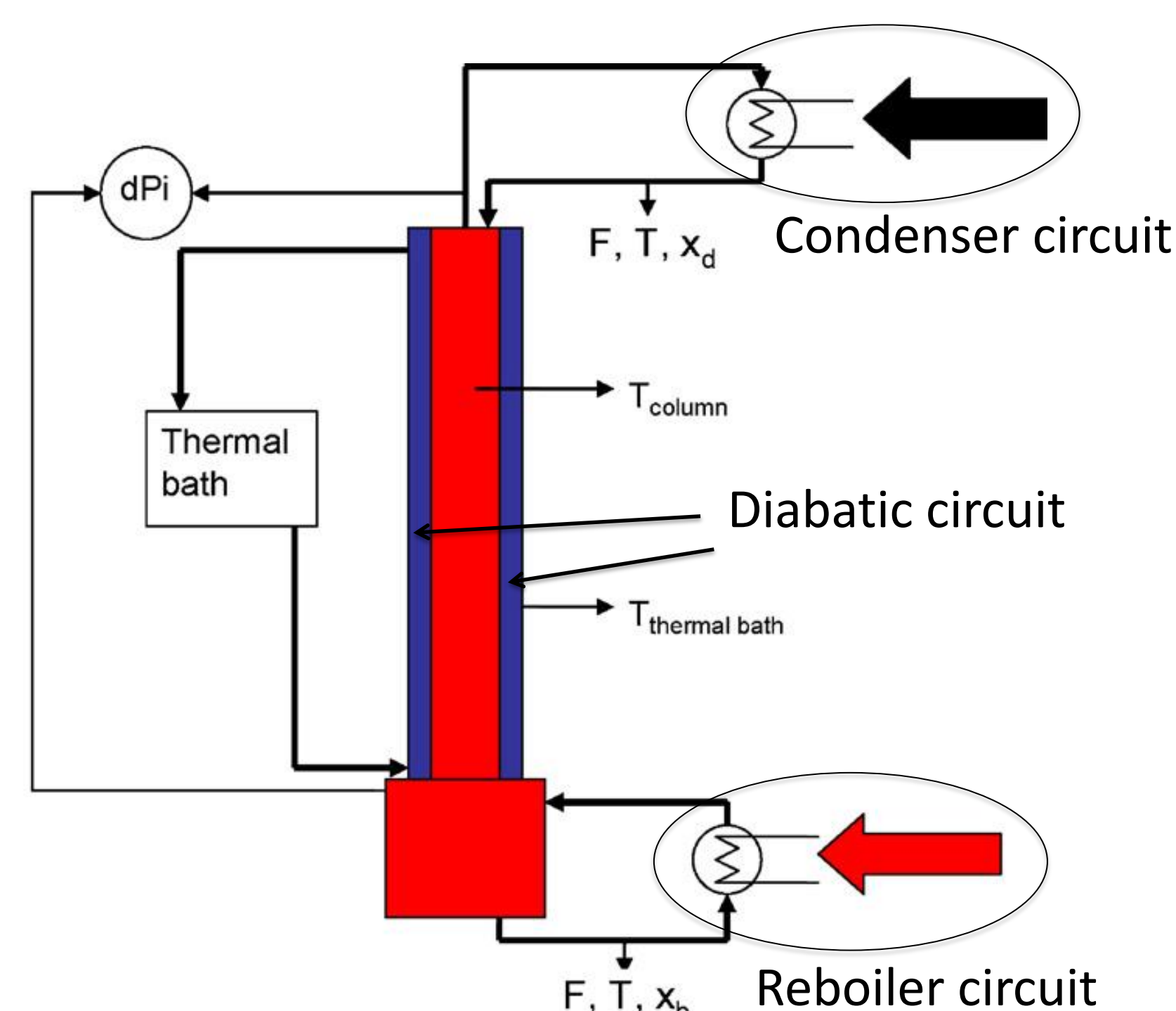


Figure 2: HIDiC (left) before insulation, flow sheet (right) showing sampling points

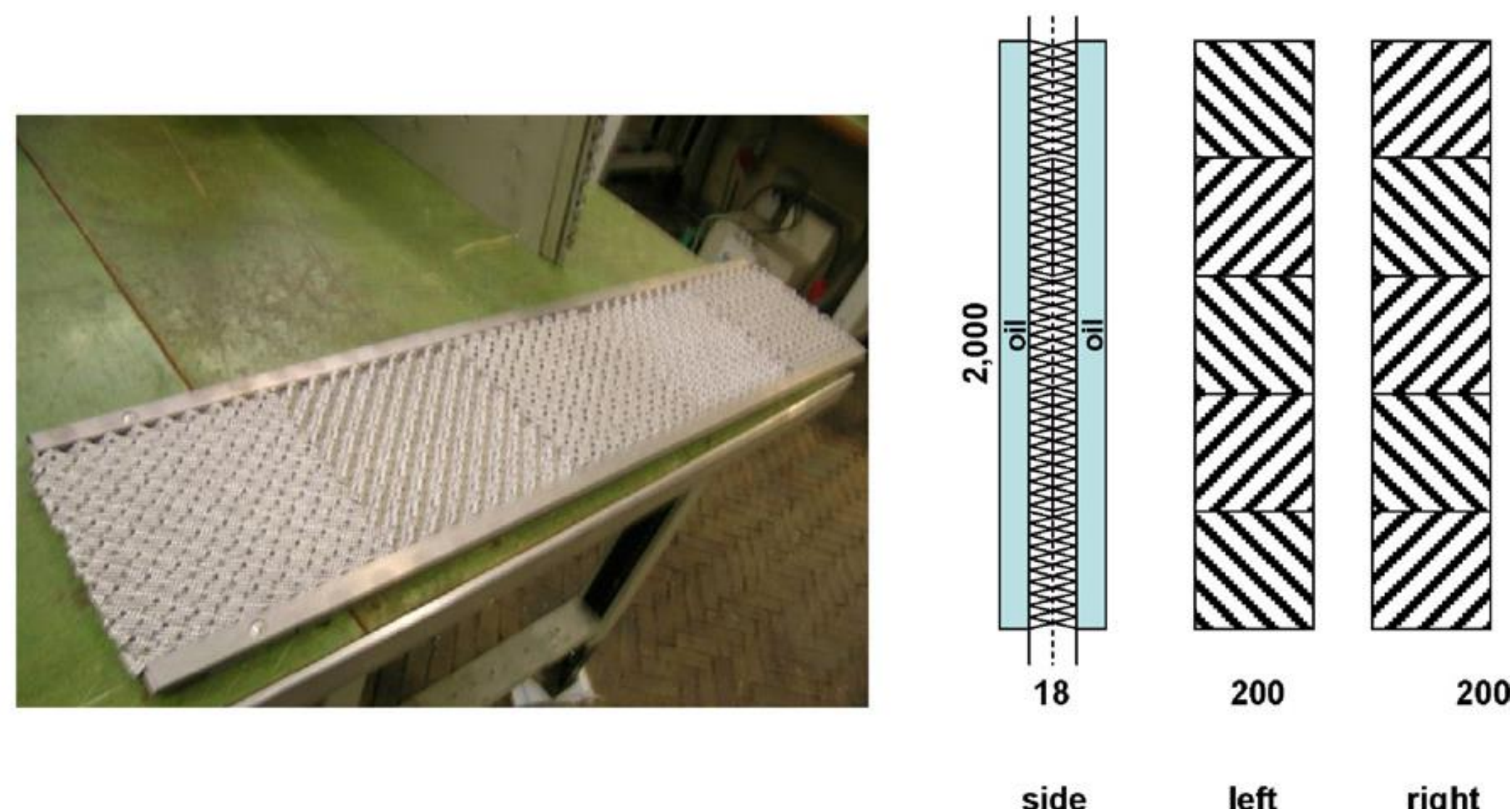


Figure 3: One side of the plate-packing and configuration details of plate packing

## Results

- The Height equivalent to a theoretical plate (HETP) is decreased and  $\Delta P$  increased when load (F-factor) increased (Figure 5, Figure 6)
- The heat transfer coefficient is fairly insensitive to changes in load
- Primary energy usage is 80 % lower than in conventional columns (Table 1) calculated from heat transfer (Figure 4)

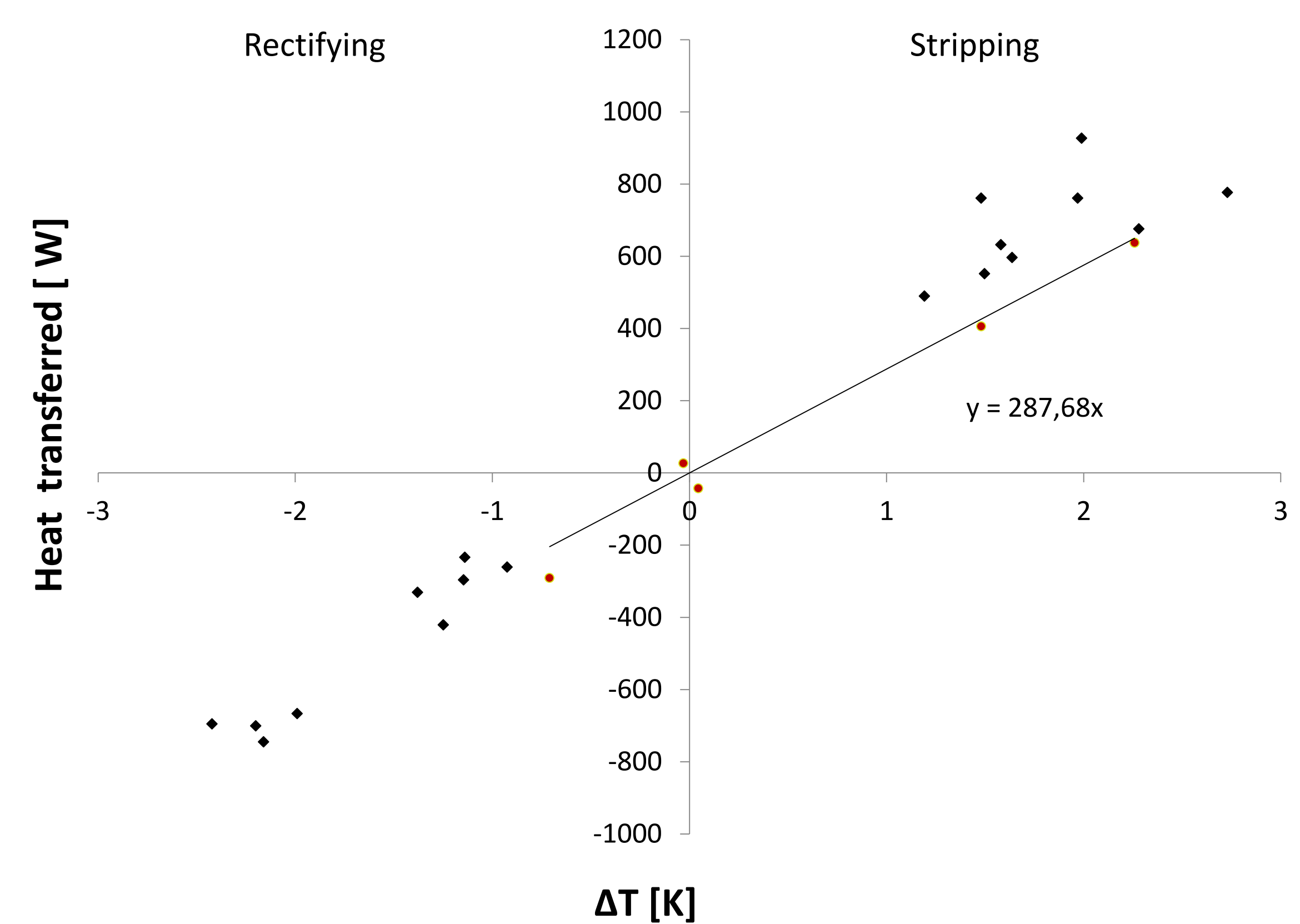


Figure 4: Heat transferred in HIDiC for rectifying and stripping mode as a function of  $\Delta T$

Table 1: energy and economic data

| Column                         | Conv. Col. | PP-HIDiC |
|--------------------------------|------------|----------|
| F-factor [ $\text{Pa}^{0.5}$ ] | 1.81       | 1.6      |
| $Q_R$ [MW]                     | 2.12       |          |
| $W_{\text{comp}}$ [MW]         |            | 0.19     |
| Prim. Energy [MW]              | 2.49       | 0.59     |
| CAPEX [k€]                     | 468        | 1393     |
| OPEX [k€/y]                    | 536        | 104      |
| PBP [y]                        | -          | 2        |

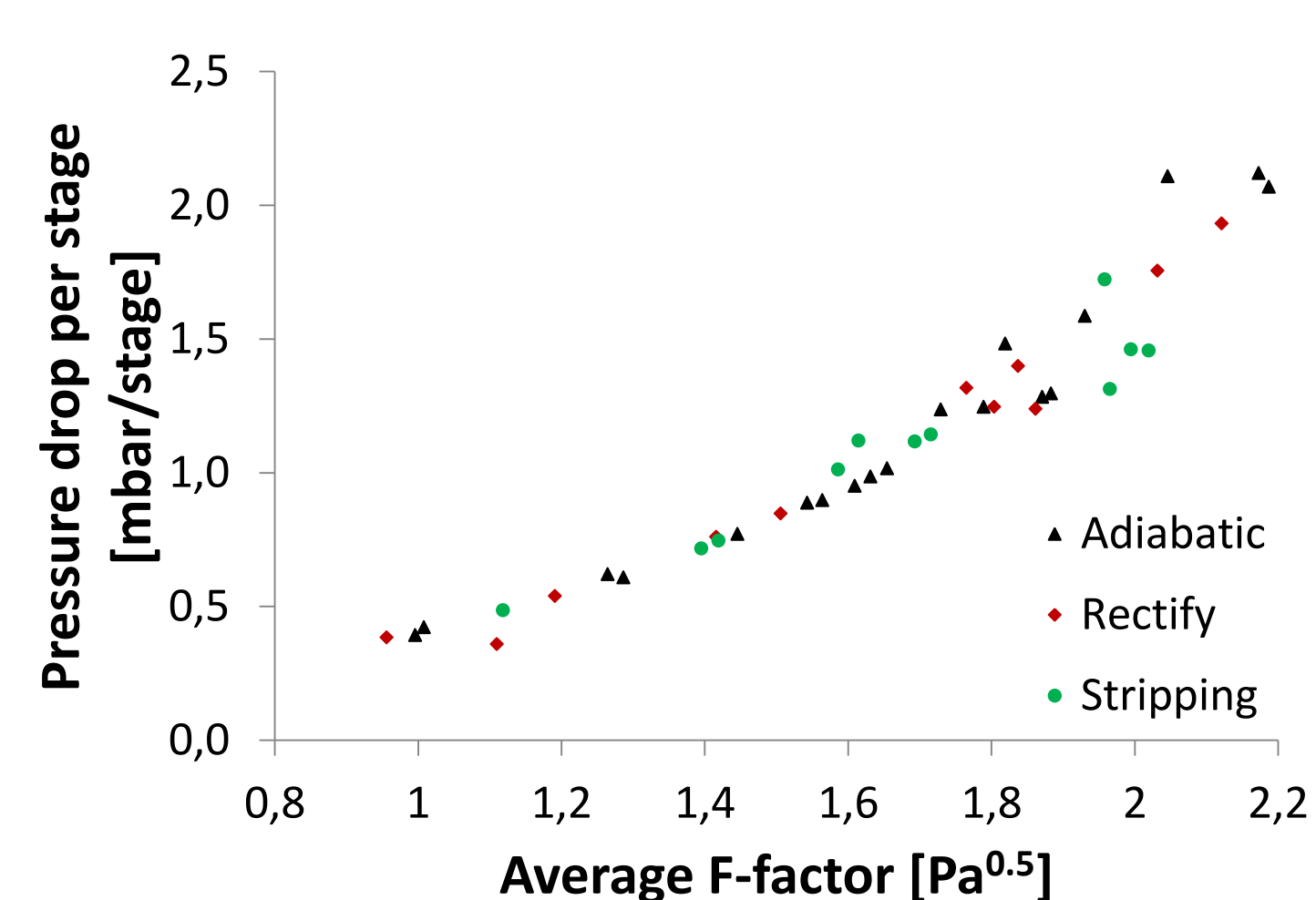


Figure 5:  $\Delta P$ /stage in 3 different modes with increasing load

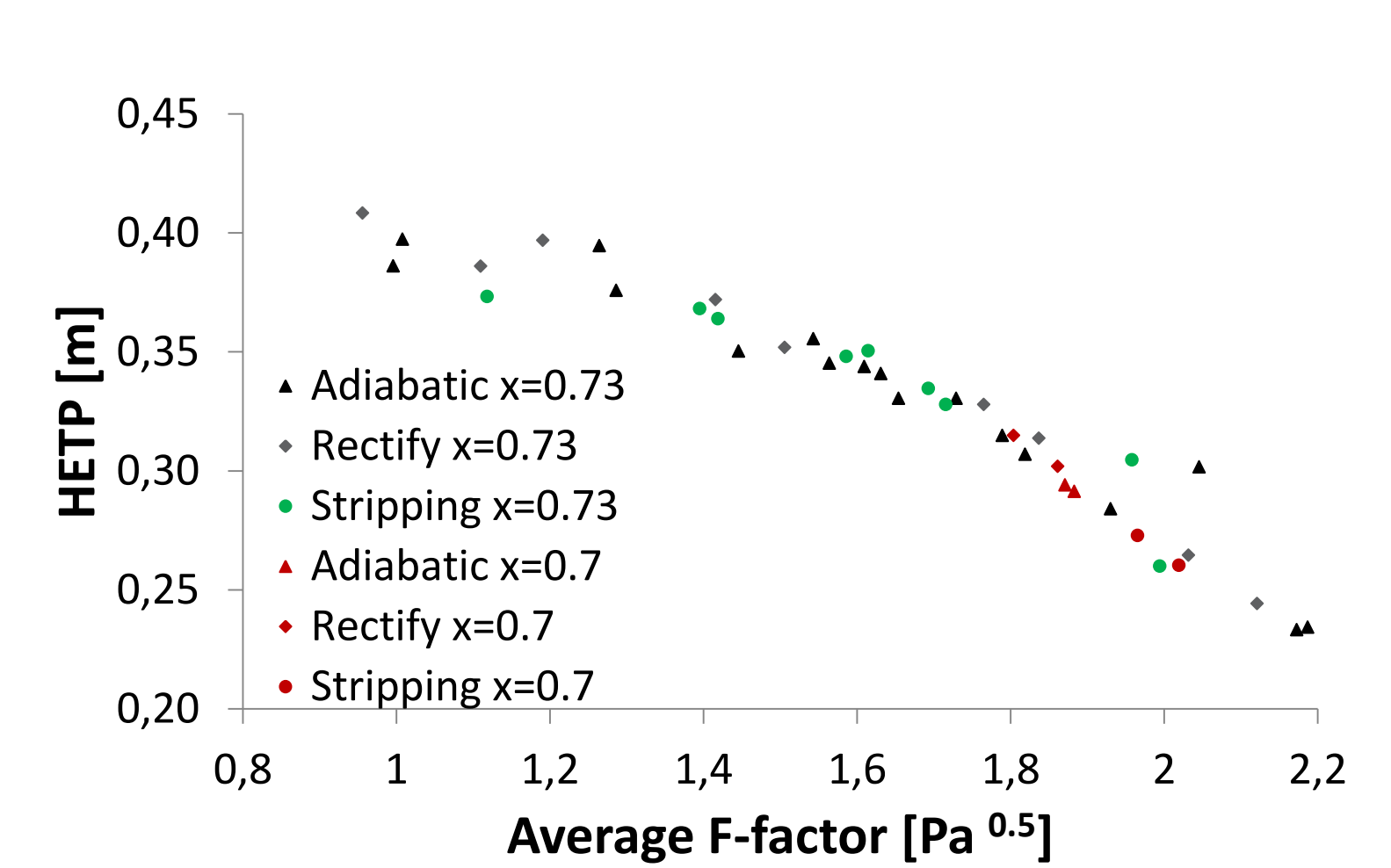


Figure 6: HETP in 3 different modes with increasing load

## Conclusion

- Structured packings have been experimentally shown to have excellent mass and heat transfer properties, which make them suitable for heat integrated distillation columns (HIDiC)
- HETP of 0.34 m and pressure drop of 0.95 mbar/stage were measured
- Energy efficiency improvement over conventional columns can be as high as 80 %
- The payback times for HIDiC columns can be as low as 2 years
- Structured HIDiC extends the application of heat pumps in distillation from close boiling mixtures to a  $\Delta T$  of 40 - 50 °C

## References

1. A. Kiss and O. Žarko. "A review on process intensification in internally heat-integrated distillation columns". Chem Eng Proc 86 (2014) 125.
2. O.S.L. Bruinsma et.al, "The Structured heat integrated distillation column". Chem Eng Res Des 90 (2012) 458.



**ECN**

Westerduinweg 3  
1755 LE Petten  
The Netherlands

P.O. Box 1  
1755 LG Petten  
The Netherlands

T +31 88 515 4949  
F +31 88 515 8338  
info@ecn.nl  
www.ecn.nl